

376a enters microchannel distillation section **370a** and flows along interior wall **371a** as a thin film, as indicated by arrow **373a**, until it contacts capture structure **372a**. The vapor phase flows through capture structure **372** into microchannel distillation section **370a**, as indicated by arrow **312**, and flows through microchannel distillation section **370a** until it contacts capture structure **372a**. The vapor phase flow may be driven by a pressure differential. Within microchannel section **370a**, the liquid phase and the vapor phase contact each other. Part of the more volatile component **Y** transfers from the liquid phase to the vapor phase to form a component **Y** rich vapor phase. Part of the less volatile component **X** transfers from the vapor phase to the liquid phase to form a component **X** rich liquid phase. The vapor phase flows through capture structure **372a** into microchannel distillation section **370b**, as indicated by arrow **313**. The liquid phase flows from capture structure **372a** through liquid outlet **374a** through flow passages in the wicking region **332** in liquid channel **330**, as indicated by arrow **335**, into liquid inlet **376**. The liquid phase flows through liquid inlet **376** into microchannel distillation section **370** and along interior wall **371** as a thin film, as indicated by arrow **373**, until it contacts capture structure **372**. The vapor phase flows into microchannel distillation section **370**, as indicated by arrow **311**, and flows through microchannel distillation section **370** until it contacts capture structure **372**. Within the microchannel distillation section **370** the liquid phase and the vapor phase contact each other. Part of the more volatile component **Y** transfers from the liquid phase to the vapor phase to form a component **Y** rich vapor phase. Part of the less volatile component **X** transfers from the vapor phase to the liquid phase to form a component **X** rich liquid phase. The component **X** rich liquid phase flows from capture structure **372** through liquid outlet **374** into liquid channel **330**, as indicated by arrow **336**. The liquid phase flowing along line **336** has a higher concentration of component **X** and a lower concentration of component **Y** than the liquid phase flowing downwardly through liquid channel **330** into liquid inlet **376b**, as indicated by arrow **333**. The vapor phase flowing through capture structure **372b**, as indicated by arrow **314**, has a higher concentration of component **Y** and a lower concentration of component **X** than the vapor phase entering microchannel distillation section **370**, as indicated by arrow **311**. Within the liquid channel **330** the more volatile component **Y** may vaporize and form vapor bubbles that rise upwardly through the wicking region in the liquid channel **330**. This vapor may be drawn into one or more of the microchannel distillation sections (**370**, **370a**, **370b**) through the liquid inlets (**376**, **376a**, **376b**) and combined with the vapor phase flowing through the microchannel distillation sections (**370**, **370a**, **370b**). Heat exchange fluid flows through heat exchange channels **350** and **360** in a direction that may be co-current or counter-current to the flow of the vapor phase through the process microchannel **310**. In one embodiment, the flow of heat exchange fluid through heat exchange channel **350** could be in one direction and the flow of heat exchange fluid through heat exchange channel **360** could be in the opposite direction. The heat exchange fluid heats the process fluids in the process microchannel **310** and the liquid channel **330**.

[0060] The microchannel distillation unit **300A** illustrated in FIG. 5 is identical in design and operation to the microchannel distillation unit **300** illustrated in FIG. 4 with the exception that the microchannel distillation unit **300A**

provides for the flow of the heat exchange fluid in a cross-current direction relative to the flow of the vapor phase through the process microchannel **310**.

[0061] The microchannel distillation unit **300B** illustrated in FIG. 6 is identical in design and operation to the microchannel distillation unit **300** illustrated in FIG. 4 with the exception that the microchannel distillation unit **300B** employs supplemental vapor channels **380** and **386**, and compressor **390**. Vapor channel **386** is adjacent to heat exchange channel **350**. Vapor channel **380** is adjacent to vapor channel **386**. Each of the micro distillation sections (**370**, **370a**, **370b**) has a supplemental vapor inlet, for example, a channel or tube (**382**, **382a**, **382b**) extending from the vapor phase channel **380** to the process microchannel **310**. Each of the microchannel distillation sections (**370**, **370a**, **370b**) also has a supplemental vapor outlet, for example, a channel or tube (**384**, **384a**, **384b**) extending from the process microchannel **310** to the vapor phase channel **386**. The vapor phase channels **380** and **386** may be microchannels, and each may have the same dimensions as the process microchannel **310** or the liquid channel **330**. The operation of the microchannel distillation unit **300B** is the same as the microchannel distillation unit **300** with the exception that the vapor phase is recirculated through the microchannel distillation unit **300B** as a vapor phase rather than being condensed and recirculated through the microchannel distillation unit **300** as a liquid phase. The vapor phase flows from compressor **390**, as indicated by arrows **393**, through vapor phase channel **380**, and from vapor phase channel **380** through each of the vapor phase inlet channels or tubes (**382**, **382a**, **382b**) into each of the microchannel distillation sections (**370**, **370a**, **370b**) where it combines with vapor phase flowing from reboiler **130**, vapor phase flowing from reboiler **130** being indicated by arrows **311**, **312**, **313** and **314**. In the microchannel distillation sections (**370**, **370a**, **370b**) the vapor phase contacts the liquid phase flowing along the interior walls (**371**, **371a**, **371b**). The liquid phase and the vapor phase undergo a mass transfer in each of the distillation sections (**370**, **370a**, **370b**) as described above. Part of the vapor phase flows through the capture structure (**372**, **372a**, **372b**) and part of the vapor phase exits the microchannel distillation sections (**370**, **370a**, **370b**) through the vapor phase outlet channels (**384**, **384a**, **384b**) and flows into vapor phase channel **386**. The vapor phase flows from vapor phase channel **386** back to compressor **390** as indicated by line **394**.

[0062] In one embodiment, a microchannel distillation unit that may be used in any of the above-described distillation columns, including distillation columns **100** and **100A**, may have the construction illustrated in FIG. 7. Referring to FIG. 7, microchannel distillation unit **400** comprises: liquid channel **415**; process microchannels **420**, **425**, **420a** and **425a**; vapor channels **435**, **440**, **445**, **435a**, **440a** and **445a**; vapor inlet/outlets **450**, **452** and **454**; and heat exchange channels **470** and **475**. Liquid channel **415** contains wicking region **416**. The microchannel distillation unit **400** illustrated in FIG. 10 comprises two microchannel distillation sections, namely, microchannel distillation sections **410** and **410a**. It will be understood, however, that although the illustrated embodiment depicts two microchannel distillation sections, the microchannel distillation unit **400** may comprise any desired number of microchannel distillation sections, for example, three, four, five, six, seven, eight, ten, tens, hundreds, thousands, etc. Each of the